



Review

Aquaculture and agriculture-by products as sustainable sources of omega-3 fatty acids in the food industry

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ABSTRACT

The valorization of by-products is currently a matter of great concern to improve the sustainability of the food industry. High quality by-products derived from the food chain are omega-3 fatty acids, being fish the main source of docosahexaenoic acid and eicosapentaenoic acid. The search for economic and sustainable sources following the standards of circular economy had led to search for strategies that put in value new resources to obtain different omega-3 fatty acids, which could be further employed in the development of new industrial products without producing more wastes and economic losses. In this sense, seeds and vegetables, fruits and crustaceans by products can be an alternative. This review encompasses all these aspects on omega-3 fatty acids profile from marine and agri-food by-products together with their extraction and purification technologies are reported. These comprise conventional techniques like extraction with solvents, cold press, and wet pressing and, more recently proposed ones like, supercritical fluids fractionation and purification by chromatographic methods. The information collected indicates a trend to combine different conventional and emerging technologies to improve product yields and purity. This paper also addresses encapsulation strategies for their integration in novel foods to achieve maximum consumer acceptance and to ensure their effectiveness.

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1. INTRODUCTION

There is an increased consumer request towards foodstuffs which provides health benefits. Lipids play an important role in the storage of energy and are essential in the membrane constitution. The different lipid diet sources have different significance owing to their composition of fatty acids (FA) which range between 2 and 36 carbon atoms. In animal and plant fats, FA are mainly present in a chain-length of 14-22 carbon atoms, with 0-6 double bonds [1]. Depending on their degree of saturation in the carbon chain, they can be divided into saturated fatty acids (SFAs) if no double bonds are present, monounsaturated fatty acids (MUFAs) with only one double bond and polyunsaturated fatty acids (PUFAs), if two or more double bonds are present (Figure 1) [2]. Within the PUFAs, two main groups called omega-3 (ω 3) and omega-6 (ω 6) FA are essential FA (EFAs) for humans because they are unable to biosynthesize them. The two major ω 6 PUFAs consumed in the diet are linoleic acid (18:2; ω 6; LA) and arachidonic acid (20:4; ω 6; ARA) and the three main ω 3 PUFAs are α -linolenic acid (18:3; ω 3; ALA), eicosapentaenoic acid (20:5; ω 3; EPA), and docosahexaenoic acid (22:6; ω 3; DHA) [3, 4]. ALA (18:3; ω 3) should

be differentiated from γ -linolenic acid (GLA) that is also 18:3 but an ω 6 FA [4]. The ω 3 FA are important nutrients with potent health benefits for the human body and brain. They act on the immune and nervous systems, being essential for the maintenance of normal brain function and also act on the cardiovascular system due to its antithrombotic and antiarrhythmic effects [5, 6]. Recommendations for minimum dietary intake of EPA plus DHA vary between 250-450 mg/day, especially for pregnant women and those of reproductive age [1]. In this sense, the increased demand for products preventing from cardiovascular diseases in combination with EPA and DHA essential supplementation due to non-synthesis in human body, makes the development ω 3 FAs an important product to establish in European nutraceutical markets [7]. Besides, in the current Covid-19 pandemic situation, the employment of ω 3 supplements can be considered as a supportive therapy and a prevention strategy in SARS-Cov-2 infection, managing the “cytokine storm” and treating the cardiovascular complications associated to the illness [8]. Also, there is an evidence to suggest that n-3 PUFAs play a role in depression and mental disorders affecting mood population [9]. Thus, the demand for ω 3 rich products is increasing worldwide and is expected to continuing growing.

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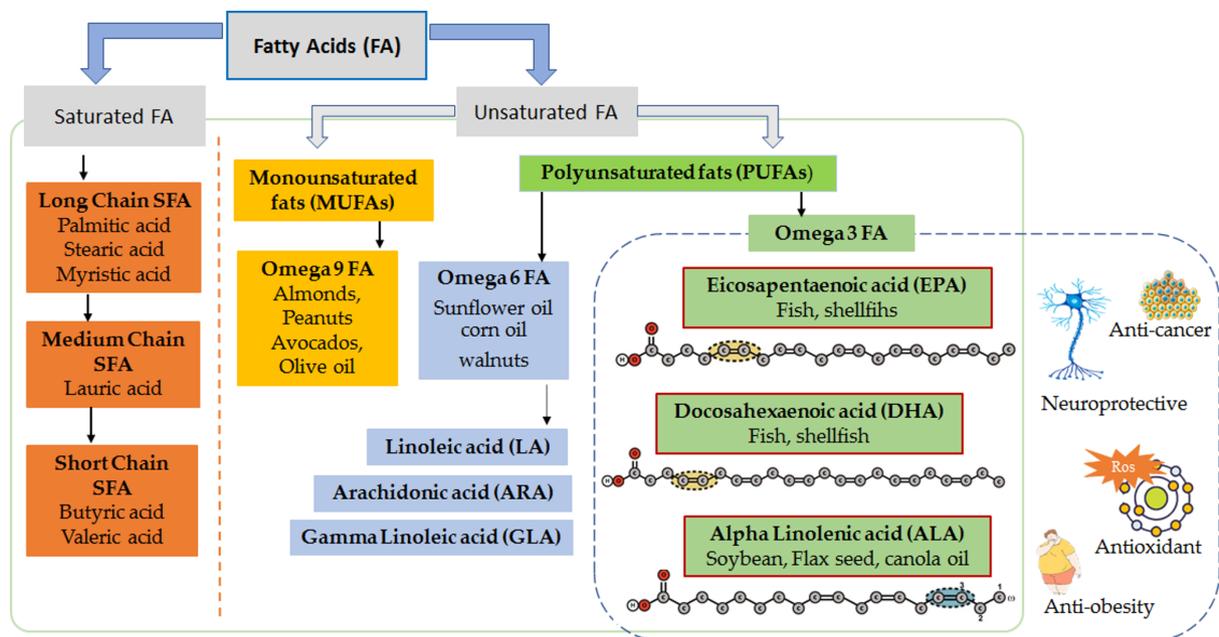


Figure 1 Fatty acids classification and main food sources.

Up to now, fish oil is considered the main source for $\omega 3$ FA production (especially those from sardines and anchovy), although alternative sources based on algae have reached the market [10, 11]. For example, Omega 3 Vegan Lineavi, a dietary supplement product containing extracts of *Schizochytrium* sp. algae oil is sold as a vegan friendly source of the healthy fats. The first attempts to collect $\omega 3$ rich oil were connected to fishery and thus today many companies selling product lines based on $\omega 3$ FAs have their origin in the fishing sector. For instance, the Norway company GC Rieber Oils were manufacturing fish oil until it started focusing on the production and commercialisation of $\omega 3$ rich products under the brand VivoMega™ in 2011. Thus, the global market for $\omega 3$ FA is dominated by products derived from fish oil and most products on the market contain combinations of DHA and EPA as both FA are present in fish oil representing a higher market share than from vegetable sources being rich in ALA [12]. Aquaculture is the sector that consumes the most fish oil, accounting for about 70% of global demand [13]. Whereas only a small fraction (5%) of global fish oil production is used to produce functional food for humans.

The $\omega 3$ FA markets have an important challenge related to the rising prices of fish oils due restrictions on fishing in high sea areas or the increasing aquaculture cost [14]. The use of fish oil as the main source for $\omega 3$ products has to be reduced in the upcoming years, due to more sustainable and cheaper plant-based sources, like nuts and seeds (e.g. chia or flax seeds, canola and soybean-based) [15]. Also, other fish species as well as crustaceans and mollusks can be an alternative [16, 17]. To meet sustainable optimisation strategies and further focus on high value PUFAs, new process and productions are being investigating. One example is the company Cargill from US together with the German BASF 29 BASF which have designed in 2016 the $\omega 3$ rich canola oil, an alternative to fish oil in aquaculture feed, commercialising under concentrated $\omega 3$ FA powders (Dry n-3 Powders).

In parallel, the production of foods worldwide has increased quickly due to the growing population in the recent decades [18]. Consequently, the production of food waste has also increased, leading to serious environmental problems. In this sense, the valorization of food by-products for the recovery of high-added value compounds has gained attention in the recent years as an alternative to reduce wastes (García-Oliveira et al., 2020b) and several studies have reported the satisfactory recovery of diverse compounds from food by-products, including FA [19]. Following this trend, the present paper aims to critically review sustainable strategies for obtaining high quality FAs from by products, not only from fish but also crustaceans, cereals, fruits, and vegetables, following the green extraction technologies, the target FA and their encapsulation for their re-integration in the food systems. The oil can be encapsulated in so called soft-gel capsules or used as it is for being incorporation into other complex nutrient systems for dietary supplementation [20]. Fisheries produce a large quantity of by-products, which can be classified into solid waste (heads, shells, tails, fins, viscera and shells and shellfish waste) and liquids (wastewaters produced during processing). Besides, agriculture by-products are sources of oils and FA, which can be widely applied for extraction or nutraceutical preparation. It is a fact that fish oil is a well-established source for $\omega 3$ FA supplementation and therefore, alternative sources may need more time to replace those on the market [21, 22]. This has happened with companies producing $\omega 3$ FA from microalgae which had to invest in research and inform potential stakeholders and consumers about the positive impact of their products.

2. LIPID COMPOSITION OF AQUACULTURE AND AGRICULTURE-BY PRODUCTS

Currently, different varieties of food by-products are considered as a promising source of FA. In general terms, those by-products containing very high proportions of FA and consequently, the most

studied are those obtained from fish (blue fish, white fish, and semi-fat fish), crustacean, cereals, fruits and vegetables. Furthermore, the predominant type of FA varies depending on the food, being fish and crustacean rich in PUFA such as EPA, DHA, whereas cereals, fruits and vegetables are rich in oleic acid (OA), palmitic acid (PA) and ALA [23].

2.1. Fish, crustacean and mollusks by-products

According to FAO, the amount of fisheries waste has grown in recent years, reaching 9.1 million tons in 2019. Considering this situation, these by-products are becoming a global concern and it is clearly necessary to reduce the amount of waste to guarantee the sustainability of fishing sector [24]. It has been estimated that fish processing generates diverse by-products, corresponding to a 15% of fish weight when gutting and scaling and even a 70% when filleting. Generally, these by-products are discarded and incinerated, but they have been also used for animal feed or biofuel production [25, 26]. However, numerous studies have found that fish by-products contain high concentrations of ω 3 FAs (EPA and DHA) which exhibit beneficial health effects [27], so that fishing industries are interested in utilizing those by-products to extract these high-value compounds with the aim of their further use in different areas, such as nutritional supplements or functional foods [24]. Table 1 shows the major FA present in different by-products from fish species, being, among others, liver, viscera, trimming, skin, head and eyeball the most analyzed ones. According to total fat amount, fish can be divided into three great types: i) white fish or lean fish, ii) semi-fat fish and, iii) blue fish or fatty/oily fish. Cod, haddock, or tusk are some examples of white fish. They are known to contain lower fat concentrations and ω 3 FA proportions than blue fish. For example, Falch and co-workers studied the FA composition in liver, viscera and trimming by-products of gadiform species (cod, haddock, saithe, tusk, and common ling) [28]. These authors found EPA and DHA in all those wastes, being viscera and trimming by-products the ones with the highest proportion of DHA (between 5.1-32.8%) (Table 1). Comparing species, the highest DHA content was found in saithe trimming by-products (ling viscera and trimming) in which it was equal to 60-70% of total PUFA. On the other hand, EPA content was similar in all by-products of gadiform species. Their ranges varied between 3.6-13.3% and are equal to 11-35% of total PUFA (Table 1). Regarding blue fish, salmon, sardine or tuna are some examples of fatty fish, which are very rich in ω 3 FA. Several studies found important amounts of EPA, DHA, PA and OA in liver, head, eyeball, viscera and skin of tuna, salmon and sardinella (Mkadem & Kaanane, 2019a) (Table 1). The highest EPA proportion was for sardine by-products, in which its proportion was about 22%, representing a 57% of total PUFA, following by sardinella species (skin, 10.4- 20.5%) [29] and Atlantic Salmon (viscera, 8.5%) [27] (Table 1). Finally, semi-fat fish contains intermediate proportions between blue and white fish. For instance, Watanabe and colleagues showed that liver of bonito is rich in PUFA, being between 50 and 60% of total FA, in which 8-15% correspond to EPA and 30-33% to DHA [30]. In this same study, the authors studied bonito by-products (heart, stomach, spleen, gonad and pyloric cecum) composition resulting in high proportions of DHA (about 30% of total FA) (Table 1). Likewise, high content of MUFA such as OA and

SFA such as PA has been also found in fish, being the range between 9-44% for OA and between 13-22% for PA. Stearic acid (SA) was found in low proportions (about 3.8 and 7%) in salmon, sardine and tuna by-products (Table 1).

Regarding crustacean, it has been described that around a 60% of the total body weight corresponds to the exoskeleton and heads, leaving only 40% of the weight destined for consumption [31]. There are less studies focus on obtaining FA from their by-products, since they usually contain lower PUFA, MUFA and SFA proportions than fish. For example, one study reported that heads, shells and tails of shrimp contain about 10% of EPA and DHA and up to 15% of PA and 10% of OA [32]. Similar results were also showed for snow crab, being EPA and DHA the 40% and 35% of total PUFA, respectively; while PA corresponded to a 38% of total SFA and OA the 18% of total MUFA [33] (Table 1). Finally, also few studies evaluating the FA profile of mollusks by-products (shells, viscera and heads) have been found in the literature. Recently, a study checked the FA profile of waste from *Octopus tetricus* (*O. tetricus*) and *Septoteuthis australis* (*S. australis*) [34] (Table 1). Both species were rich in PUFA, being DHA and EPA the main FA of this group, with values of 14.19% and 12.3% in *O. tetricus* and 5.3% and 20.6% in *S. australis*, respectively. These by-products also contained significant amounts of SFA such as PA and SA. Specifically, in *O. tetricus*, PA and SA corresponded to the 13.2% and 6.9% of the total FA, while in *S. australis*, the content of these two FA was 17.6% and 6.7%, respectively. Both species showed a low MUFA content, with OA as the main FA and present in values under 6% [34] (Table 1).

2.2. Cereal's by-products

Nowadays, the production of cereals worldwide is enormous. Just to cite an example, UE produces about 156 million of tons of wheat and 7 million of tons of oat every year. As expected, the wastes derived for this production are also enormous, which are about 25% of total production of cereals [35]. These by-products are considered as an underexploited resource, which presents compounds with good nutritional values and could be used in food industry, animal feed and in bioethanol production. Various studies reported important FA concentrations in cereal by-products, awakening the interest of the food industries to re-value these residues [36–38]. Table 1 shows the FA profile of different cereal by-products. According reported studies, the most used by-product is the bran, consisting in the coat seeds and aleurone layer from the grinding of the cereal grains, after separating the endosperm. The bran contains an oily fraction rich in LA, PA and OA, but also ALA and SA in lower concentrations, ranging between 5-11% for ALA and between 1-7% for SA. Many studies show the FA profile of the bran oil in different cereals such as wheat, rice, oat, corn, rye and spelt (Table 1). LA is the most predominant compound with more 50% of total FAs and is equal to 90-95% of total PUFA in all bran oils of cereals, except in rice and oat bran oil, in which LA proportion is below 40% of FAs.

Table 1 FA profile in different food by-products.

Product	By-product	FA	Chemical structure	FA amount	Type FA and total content	Detection method	Ref
FISH							
Cod (<i>Gadus morhua</i>)	Liver	EPA, DHA		5.8-10.1%, 6.0-15.2%	∑ PUFA= 34.9%		
	Viscera	EPA, DHA		7.4-13.3%, 8.5-22.0%	∑ PUFA= 38.1%		
	Trimming	EPA, DHA		6.7-11.5%, 8.9-23.3%	∑ PUFA= 40.4%		
Haddock (<i>Melanogrammus aeglefinus</i>)	Liver	EPA, DHA	20:5 ω3, 22:6 ω3	9.0-13.5%, 5.6-14.1%	∑ PUFA= 37.8%	GC	[28]
	Viscera	EPA, DHA		7.7-15.7%, 10.3-20.2%	∑ PUFA= 50.7%		
	Trimming	EPA, DHA		5.4-15.3%, 10.4-25.1%	∑ PUFA= 39.0%		
Saithe (<i>Pollachius virens</i>)	Liver	EPA, DHA		4.4-7.2%, 5.1-9.4%	∑ PUFA= 33.3%		
	Viscera	EPA, DHA		5.0-10.2%, 5.9-21.9%	∑ PUFA= 41.9%		
	Trimming	EPA, DHA		7.3-11.4%, 9.5-32.8%	∑ PUFA= 47.8%		
Tusk (<i>Brosme brosme</i>)	Liver	EPA, DHA		6.7-7.8%, 9.0-10.9%	∑ PUFA= 26.6%		
	Viscera	EPA, DHA		5.6-8.5%, 7.2-18.9%	∑ PUFA= 37.2%		
	Trimming	EPA, DHA		3.6-7.4%, 8.3-16.5%	∑ PUFA= 31.8%		
Common ling (<i>Molva molva</i>)	Liver	EPA, DHA		4.8-6.6%, 5.4-9.4%	∑ PUFA= 30.8%		
	Viscera	EPA, DHA		7.8-9.3%, 8.7-28.1%	∑ PUFA= 43.9%		
	Trimming	EPA, DHA		6.2-9.3%, 6.9-28.1%	∑ PUFA= 40.2%		
Seabass (<i>Cephalopholis taeniops</i>)	Skin	DHA	22:6 ω3	6.9%	∑ PUFA= 17.5%	GC-MS	[29]
		PA	16:0	28.4%	∑ SFA= 46.4%		
		OA	18:1 cis-9	12.5%	∑ MUFA= 33.6%		
Bonito (<i>Euthynnus pelamis</i>)	Liver	PA	16:0	33.9%	∑ SFA= 58.6%	GC	[30]
		EPA, DHA	20:5 ω3, 22:6 ω3	8.16-15.07%, 30.80-32.91%	∑ PUFA= 51.56-61.11%		
		PA	16:0	14.24-20.57%	∑ SFA= 26.2-32.07%		
	Heart	DHA	22:6 ω3	33.9%	∑ PUFA= n.a		

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Table 1 continued

	Pyloric cecum	DHA	22:6 ω 3	32.7%	\sum PUFA: n.a		
	Stomach	DHA	22:6 ω 3	29.6%	\sum PUFA: n.a		
	Spleen	DHA	22:6 ω 3	28.3%	\sum PUFA: n.a		
	Gonad	DHA	22:6 ω 3	30.1%	\sum PUFA: n.a		
		EPA, DHA	20:5 ω 3;	5.2%, 21.8%	\sum PUFA= 38.2%		
Yellowfin tuna (<i>Thunnus albacares</i>)	Head		22:6 ω 3				
		PA, SA	16:0, 18:0	21.4%, 6.9%	\sum SFA= 32.3%	GC	[39]
		OA	18:1 cis-9	15%	\sum MUFA= 26.2%		
EPA, DHA	20:5 ω 3;	5.1%, 22.0%	\sum PUFA= 38.2%				
	Eyeball		22:6 ω 3				
		PA, SA	16:0, 18:0	21.1%, 6.7%	\sum SFA= 31.6%		
		OA	18:1 cis-9	16%	\sum MUFA= 27.4%		
Madeiran sardinella (<i>Sardinella maderensis</i>)	Skin	EPA	20:5 ω 3	20.5%	\sum PUFA= 33.6%		
		PA	16:0	20.5%	\sum SFA= 41.5%		
		PA	16:0	25.6%	\sum SFA= 38.0%		
	Liver	OA	18:1 cis-9	27.2%	\sum MUFA= 44.2%		
		EPA	20:5 ω 3	10.4%	\sum PUFA= 22.5%	GC	[29]
		PA	16:0	20.5%	\sum SFA= 40.3%		
	OA	18:1 cis-9	15.5%	\sum MUFA= 34.0%			
Round sardinella (<i>Sardinella aurita</i>)	Skin	PA	16:0	23.2%	\sum SFA= 32.3%		
		OA	18:1 cis-9	44.7%	\sum MUFA= 54.0%		
		EPA, DHA, ALA	20:5 ω 3,	22.28%, 6.71%,	\sum PUFA= 38.91%		
	Liver		22:6 ω 3,	2.36%		GC	[40]
			18:3 ω 3				
		PA, SA	16:0, 18:0	19.57%, 3.82%	\sum SFA= 34.71%		
	Atlantic salmon (<i>Salmo salar</i>)	OA	18:1 cis-9	11.42%	\sum MUFA= 24.66%		
		EPA, DHA, DPA,	20:5 ω 3;	8.5%, 6.6%, 3.7%,	\sum PUFA= 31.9%	GLC	[27]
		LA	22:6 ω 3,	4.4%			
		22:5 ω 3,					
		Myristic, PA, SA	14:0, 16:0,	7.1%, 18.8%, 4.8%	\sum SFA= 30.8%		
			18:0				
		OA	18:1 cis-9	18.9%	\sum MUFA= 37.4%		
CRUSTACEAN							
Northern pink shrimp (<i>Pandalus borealis</i>)	Heads, shells and tails	EPA, DHA	20:5w-3,	8.9%, 10.7%	\sum PUFA= 43.9%		
			22:6 ω 3				
		PA, SA	16:0, 18:0	14.8%, 5.8%	\sum SFA= 25.9%	GC	[32]
	OA	18:1 cis-9	9.3%	\sum MUFA= 29.6%			
	EPA, DHA,	20:5 ω 3;	10.7%, 10.9%	\sum PUFA= 48.3%			
	Spotted shrimp (<i>Trachypena curvirostris</i>)		22:6 ω 3			GC	
		PA, SA	16:0, 18:0	13.1%, 7.3%	\sum SFA= 26.1%		
		OA	18:1 cis-9	6.3%	\sum MUFA= 25.0%		

Continued on next page

Table 1 continued

Snow crab (<i>Chionoecetes opilio</i>)	Cephalothorax shells, digestive systems and physiological liquid	EPA, DHA	20:5 ω 3, 22:6 ω 3	9.9%, 8.9%	\sum PUFA= 24.4%	GC-FID	[33]
		PA, SA	16:0, 18:0	9.9%, 2.1%	\sum SFA= 26.1%		
		OA	18:1 cis-9	9.4%	\sum MUFA= 50.4%		
MOLLUSKS							
Octopus (<i>Octopus tetricus</i>)	Viscera	EPA, DHA	20:5 ω 3, 22:6 ω 3	12.3%, 14.19%	\sum PUFA= 40.8%	GC-FID	[34]
		PA, SA	16:0, 18:0	13.2%, 6.9%	\sum SFA= 24.9%		
		OA	18:1 cis-9	4.4%	\sum MUFA= 10.3%		
Squid (<i>Sepioteuthis australis</i>)	Head	EPA, DHA	20:5 ω 3, 22:6 ω 3	5.3%, 20.6%	\sum PUFA= 36.1%	GC-FID	[34]
		PA, SA	16:0, 18:0	17.6%, 6.7%	\sum SFA= 28.4%		
		POA, OA	16:1, 18:1 cis-9	5.5%	\sum MUFA= 7.8%		
CEREALS							
Wheat (<i>Triticum aestivum</i>)	Wheat bran oil	ALA, LA	18:3 ω 3, 18:2 ω 3	5.0-5.5%, 57.8-62.6%	\sum PUFA= 63.0 %	GC	[38, 41]
		PA	16:0	15.5-18.9%	\sum SFA= 19.2 %		
	OA	18:1 cis-9	14.6-16.4%	\sum MUFA= 17.8%			
	ALA, LA	18:3 ω 3, 18:2 ω 6	7.2-9.5%, 54-59.5%	\sum PUFA= 63.0 %			
Oat	Wheat germ oil	PA	16:0	17.1-20.3%	\sum SFA= 19.2 %	GLC	[37, 38]
		OA	18:1 cis-9	11.8-17.6%	\sum MUFA= 17.8%		
	ALA, LA	18:3 ω 3, 18:2 ω 3	0.9-1.2%, 34.6-37.8%	\sum PUFA= 35.7-38.9%			
	PA, SA	16:0, 18:0	16.5-16.9%, 1.4-1.8%	\sum SFA=18.7-18.8 %			
Rice	Rice bran oil (chemically refined)	LA	18:2 ω 3	38.5%	\sum PUFA= 39.2 %	GLC	[36]
		PA	16:0	18.7%	\sum SFA= 25.5%		
		OA	18:1 cis-9	38.3%	\sum MUFA= 38.6%		
	LA	18:2 ω 6	40.4%	\sum PUFA= 40.6%			
	PA	16:0	17.2%	\sum SFA= 20.5%			
	OA	18:1 cis-9	37.9%	\sum MUFA= 38.9 %			
Corn	Corn bran oil	ALA, LA	18:3 ω 3, 18:2 ω 6	2.4%, 59.0%	\sum PUFA= 60.2%	GC	[37]
		PA, SA	16:0, 18:0	11.4%, 1.4%	\sum SFA= 12.8%		
		OA	18:1 cis-9	27.0%	\sum MUFA= 27%		
Rye	Rye bran oil	ALA, LA	18:3 ω 3, 18:2 ω 6	7.6%, 59.3%	\sum PUFA= 67.0%	GC	[37]
		PA	16:0	13.4%	\sum SFA= 14.5%		

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Table 1 continued

Spelt	Spelt bran oil	OA	18:1 cis-9	16.9%	\sum MUFA= 18.5%	GLC	[43]
		ALA, LA	18:3 ω 3,	3.2%, 57.7%	\sum PUFA= 60.9%		
Sesame (<i>Sesamum indicum</i>)	White sesame seed (after dehulling)	PA	16:0	14.3%	\sum SFA= 16.1%	GLC	[43]
		OA	18:1 cis-9	22.0%	\sum MUFA= 22.3%		
	LA	18:2 ω 6	36.1%	\sum PUFA= 36.6%			
	PA, SA	16:0, 18:0	10.9%, 6.9%	\sum SFA= 18.9%			
	OA	18:1 cis-9	43.2%	\sum MUFA= 44.6%			
	LA	18:2 ω 6	35.6%	\sum PUFA= 36.1%			
White sesame seed (after hulling)	PA, SA	16:0, 18:0	11.4%, 6.9%	\sum SFA= 19.4 %	GLC	[43]	
	OA	18:1 cis-9	43.1%	\sum MUFA= 44.5%			
FRUITS AND VEGETABLES							
Quince (<i>Cydonia vulgaris</i>)	Quince seed oil	LA	18:2 ω 6	55.7%	\sum PUFA= 56.2%	GC	[44]
		PA	16:0	6.8%	\sum SFA= 8.3 %		
		OA	18:1 cis-9	34.0%	\sum MUFA= 35.5%		
Japanese quince (<i>Chaenomeles japonica</i>)	Quince seed oil	LA	18:2 ω 6	52.4%	\sum PUFA= 53.3%	GC-FID	[45]
		PA	16:0	9.5%	\sum SFA= 11.8%		
		OA	18:1 cis-9	33.8%	\sum MUFA= 34.9%		
Peanut	Peanut seed oil	LA	18:2 ω 6	29.3%	\sum PUFA= 30.6%	GC	[44]
		PA, SA	16:0, 18:0	9.9%, 3.3%	\sum SFA= 13.2 %		
		OA	18:1 cis-9	54.4%	\sum MUFA= 56.2%		
Grape (<i>Vitis vinifera</i>)	Grape seed oil	LA	18:2 ω 6	74.2%	\sum PUFA= 74.3%	-	[46]
		PA, SA	16:0, 18:0	6.7%, 3.8%	\sum SFA= 10.6%		
		OA	18:1 cis-9	14.8%	\sum MUFA= 14.9%		
Pear (<i>Pyrus sp.</i>)	Pear seed oil	LA	18:2 ω 6	54.0%	\sum PUFA= 54.8%	GC	[44]
		PA, SA	16:0, 18:0	9.1%, 2.1%	\sum SFA= 11.2%		
		OA	18:1 cis-9	32.1%	\sum MUFA= 34.0%		
Apple (<i>Malus communis</i>)	Apple seed oil	LA	18:2 ω 6	50.3%	\sum PUFA= 51.2%	GC	[44]
		PA, SA	16:0, 18:0	6.9%, 2.0%	\sum SFA= 8.9%		
		OA	18:1 cis-9	38.3%	\sum MUFA= 40.2%		
Tomato (<i>Solanum lycopersicum</i>)	Tomato seed	LA	18:2 ω 6	40.2%	\sum PUFA= 40.6%	GC	[47]
		PA	16:0	20.2%	\sum SFA= 30.4%		
		OA	18:1 cis-9	24%	\sum MUFA= 33%		
Olive (<i>Olea europaea</i>)	Olive seed (Green)	LA	18:2 ω 6	17.2%	\sum PUFA= 17.4%	GC-MS	[48]
		PA	16:0	17.6%	\sum SFA= 28.7		
	OA	18:1 cis-9	53.6%	\sum MUFA= 53.9%			
	LA	18:2 ω 6	17.2%	\sum PUFA= 17.3%			
Olive seed (Ride)	PA	16:0	16.0%	\sum SFA=23.4%			

Continued on next page

Table 1 continued

OA	18:1 cis-9	59.1%	\sum MUFA= 59.3%
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Abbreviations : GC: gas chromatography, MS: mass spectrometry, PUFA: polyunsaturated fatty acids, MUFA: monounsaturated fatty acids, SFA: saturated fatty acids, EPA: eicosapentaenoic acid, DHA: docosahexaenoic acid, DPA: docosapentaenoic acid, PA: palmitic acid, SA: stearic acid, OA: oleic acid, ALA: α -linolenic acid, LA: linoleic acid, n.a: not analyzed.

Table 2 Extraction of oils rich in omega-3 fatty acids by different methods from aquaculture and agricultural by-products.

Extraction Method	Conditions	By-product	Product	Lipid obtained	Ref.
Bligh & Dyer	CHCl ₃ : MeOH, 1:2, v/v, 2 min	Offal	Rainbow trout (<i>Oncorhynchus mykiss</i>)	ALA, SDA, ETA, EPA, DPA, DHA	[49]
Bligh & Dyer	CHCl ₃ : MeOH, 1:2, v/v, 2 min	Liver	Balistid fish (<i>Sufflamen capistratus</i>)	ALA, DHA, DPA, EPA	[50]
Bligh & Dyer	CHCl ₃ : MeOH, 2:1, v/v, 10 min	Tissues	<i>Sardinella longiceps</i>	ALA, DHA, DPA, EPA	[51]
Bligh & Dyer	CHCl ₃ : MeOH, 1:2, v/v, 2 min	Head, intestine and liver	<i>Sardinella lemuru</i>	DHA, DPA, EPA	[52]
SxE	n-hexane, 80°C, 8 h	Seeds	Chia (<i>Salvia hispanica</i> L.)	ALA	[53]
Folch // SxE	CHCl ₃ : MeOH, 2:1, v/v, 20 min // n-hexane, 4 h	Guts	Salmon (<i>Salmo salar</i>), red coastal eel (<i>Genipterus chilensis</i>) and yellowtail horse mackerel (<i>Seriola lalandi</i>)	ALA, DHA, DPA, EPA, ETA	[54]
MAE	100 - 40% of 1,000 W, 20 - 80 s	Liver	Catfish	EPA, DHA	[55, 56]
MAE	400 W, 120 s	Seeds	Purslane (<i>Portulaca oleracea</i>)	ALA	[57]
MAE-SxE	720 W, 13 min, n-hexane	ns	Olives <i>Aglanadou</i>	ALA	[58]
UAE	C ₄ H ₈ O ₂ , 176 W, 40 kHz, 20 - 60 min, 40 -60°C	Seeds	Chia (<i>Salvia hispanica</i> L.)	ALA	[59]
UAE	n-hexane, 250 W, 20 kHz, S/L 1:10, 25°C	Seeds	Flaxseed (<i>Linum usitatissimum</i> L.)	ALA	[60]
UAE + EAE	250 W, 20 kHz, 45°C, 30 min	Seeds	Flaxseed (<i>Linum usitatissimum</i> L.)	ALA	[61]
UAE // SxE	n-hexane, 600 W, 40.0 kHz, 49°C, 44 min // 8 h	Seeds	Seeds of <i>I. indigotica</i>	ALA	[62]
UAE + SxE	n-hexane, 65 W, 9.0 kHz, 45°C, 30 min	Germ ns	Soybean Seaweed	ALA SDA, ETA, EPA, DPA, DHA	[63]
UAE + SxE	n-hexane, 20 kHz, 50-150 W, 30 min + 70°C, 6 h	Seeds	Grape (<i>Vitis vinifera</i>)	ALA	[64]

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Table 2 continued

UAE + SxE	n-hexane, 100 W, 10 s, + 75°C	Seeds	Sunflower, rape and soybean	ALA	[65]
WP // EAE	95°C, 30 min // Papain, 60°C, 120 min	ns	Seluang fish (<i>Rasbora argyrotaenia</i>)	ALA, DHA, DPA, EPA, ETA	[66]
WP	75 - 95°C, 10 - 30 min, 140 tons/m ²	Heads	Skipjack tuna (<i>Katsuwonus pelamis</i>)	ALA, SDA, EPA, DHA	[67]
WP	50 - 90°C, 2500 kg/h	Heads, bones, tails and intestines	Rainbow trout (<i>Oncorhynchus mykiss</i>)	EPA, DHA	[68]
WP // CP // EAE	95°C, 30 min, 0.02–0.04 MPa // 5 min, 8000g // Alcalase 5%, 55°C, 2 h	Skins, heads and backbones	Salmon (<i>Salmo salar</i>)	ALA, SDA, EPA, DPA, DHA	[69]
CP // SxE	2 - 6 L/h // Petroleum-ether, 5 h	ns	Almond, apricot, cashew, hazelnut, peanut, pistachio, pecan and walnut	ALA	[70]
SxE + SC-CO ₂	Petroleum-ether, 6 h // 35 MPa, 60°C, 2 mL/min, 5 - 8 h	Flesh, skins, viscera and head	Indian mackerel (<i>Rastrelliger kanagurta</i>)	HTA, ALA, SDA, EPA, DPA, DHA	[71]
PLE	200°C, 1500 psi	Germ	Wheat	ALA	[72]
PLE + SxE	C ₃ H ₆ O ₂ , 140°C, 1 - 3 mL/min, 10 - 20 MPa, 30 min + n-hexane, EtOH, C ₃ H ₆ O ₂ , 8 h	Seeds	<i>Crambe abyssinica</i>	ALA	[73]
PLE + SC-CO ₂	45 MPa, 45°C, 40 g/min CO ₂ , 4 h	Seeds	Chia (<i>Salvia hispanica</i> L.)	ALA	[74]
HHPE + SWE	150 - 450 MPa, 10 - 20 min + 90-190°C, 5 MPa, 1 - 2.5 h	Liquid cooking effluents	Mackerel (<i>Scomber japonicus</i>)	ALA, EPA, DHA, DPA	[75]
PLE	Hexane, EtOH, C ₄ H ₈ O ₂ (50%), 80 - 160°C, 100 bar	ns	<i>Laminaria ochroleuca</i>	ALA, EPA, DHA	[76]

Continued on next page

Table 2 continued

SxE // PLE // MAE // UAE	Hexane, 8 h // Hexane, EtOH, C ₄ H ₈ O ₂ , W, 60 - 200°C, 10 min // 270 - 900 W, 1 - 2 min // 30 - 80°C, 37 kHz, 15 - 30 min	Seeds	<i>Echium plantagineum</i>	ALA, SDA	[77]
SC-CO ₂ // PLE	70°C, 210 min, 45 MPa, 2 L/min // Acetone, EtOH, W, 10.3 MPa, 70 - 120°C, 15 min	ns	Algerian <i>Thymus munbyanus</i>	ALA	[78]
SC-CO ₂ // Randall extraction	500 bar, 60°C, 10 g/min // n-hexane, 69°C, 1 h	Heads, spines and viscera	Trout (<i>Oncorhynchus mykiss</i>)	ALA, EPA, DHA, DPA, HTA	[22]
SFE	3.5 L/min, 316 bar, 10 min	ns	Sturgeon	ALA, DHA, EPA, DPA	[79]
SFE, CP, WP, EAE	25 MPa, 40°C // All: RT, 12 h; EAE: Alcalase, 0.05 w/w protein	ns	<i>Merluccius capensis</i> , <i>Hoplostethus atlanticus</i> , <i>Salmo salar</i> and <i>Dosidicus gigas</i>	ALA, DHA, EPA, DPA	[80]
SC-CO ₂	40 - 60°C, 150 - 350 atm, 0.3 ml/min, 20 min,	ns	Rainbow sardine fish (<i>Dussumieria acuta</i>)	ALA, DHA, EPA	[81]
SC-CO ₂	35 - 45°C, 150-250 bar, 27.79 g/min, 1.5 h	ns	Yellow croaker (<i>Larimichthys polyactis</i>) muscle	ALA, DHA, EPA	[82]
SC-CO ₂ // SxE	65°C, 40 MPa, 3 mL/min, 2 h // n-hexane, 6 h	Head, skin and viscera	Tuna species	SDA, EPA, DPA, DHA	[83]
SC-CO ₂	40 - 80°C, 400 bar, 10 kg/h	Seeds	<i>Cannabis sativa</i> L.	ALA	[84]
SC-CO ₂	40 - 80°C, 136 - 408 bar, 1.8 g/min, 10 min	Seeds	Chia (<i>Salvia hispanica</i> L.)	ALA	[85]
SC-CO ₂	50°C, 30 MPa, 40 g/min, 3 h	Grain	Wheat grain	ALA	[86]

Abbreviations: α -Linolenic acid (ALA), Stearidonic acid (SDA), Eicosatetraenoic acid (ETA), Eicosapentaenoic acid (EPA), Docosapentaenoic acid (DPA), Docosahexaenoic acid (DHA), hexadecatrienoic acid (HTA). Microwave-assisted extraction (MAE), Ultrasound-assisted extraction (UAE), Pressurized liquid extraction (PLE), subcritical water extraction (SWE), Supercritical CO₂ extraction (SC-CO₂), High hydrostatic pressure extraction (HHPE), Wet Pressing (WP), Soxhlet Extraction (SxE), Enzyme Assisted Extraction (EAE), Cold Pressing (CP), Not specified (ns)

The highest content of LA was found for wheat bran oil, representing the 60% of total FA and until 99.4% of total PUFA [38, 41] (Table 1). OA is also an important MUFA found in bran oils, besides, their concentration is about two times higher that of PA (except in wheat bran oil, which present similar results). The highest content of OA was reported in oat bran oil, reaching a 40.4% of total FA content [37, 42].

Regarding ALA and SA, generally, these compounds are present in very low concentrations (< 2%) in bran oils of most cereals. However, significant concentrations of the ω 3 ALA until 9.5% are found in wheat bran oil [38, 41] and in rye bran oil (7.6%) [37], while SA represented until 7% of total FA in white sesame seed oil [43] (Table 1). Another by-product from cereal production evaluated in some studies are seeds. For example, Elleuch and co-workers analyzed the FA profile of sesame seed oil after de-hulling and hulling and they reported high amounts of LA and OA (all above 30% of total FA). On the contrary, lower content of SFA was observed, with values of ALA and SA under 12% in both matrix [43] (Table 1).

2.3. Fruits and vegetables by-products

According to FAO, UE is a major producer of vegetables and fruits. To cite some examples, 10.3 million of tons of tomatoes were produced in 2018 and 1.6 million of tons of olive oil are produced every year [35]. Parallel to this production, enormous amounts of fruits and vegetables wastes are generated and more than 20% of the global production of fruits and vegetables is lost between harvest and distribution [35]. In addition, fruit and vegetable processing industry is recognized as one of the greatest producers of food by-products, reaching to discard between 15 and 60% of the total mass of the food. To reduce waste quantities and economic costs of this industry, different by-products like peels, skin, pomace or seeds have been evaluated for the recovery of diverse compounds, including FA. In this sense, most studies have used fruits and vegetable seeds to obtain FA [19, 47, 87]. In Table 1, the FA composition of different fruit and vegetable seeds has been compiled. According to these data, their FA profiles are very similar, highlighting the PUFA and MUFA fractions.

In these fractions, LA and OA are the most predominant FA, respectively, with percentages that vary between 17-74% for LA and between 14-60% for OA. Considering the compiled data, high amounts of LA are present in quince and grape seeds, with values of 55.7% and 74.2% of the total PUFA, respectively [44, 46]. On the other hand, large amounts of OA are found in olive seed and peanut seeds oil, corresponding to a 54.4% and 59.1%, respectively [44, 48] (Table 1). In addition, most studies found that about 98% of total PUFA and about 95% of total MUFA correspond to LA and OA, respectively. However, a study shows that the highest OA proportion for tomato seed oil was 72% of total MUFA [47]. Finally, the main SFA are PA and SA, which are present in low concentrations in the studied matrix, both in proportions below 10%, except in tomato and olive by-products, in which the percentage of PA varies between 16%-20% (Table 1). Generally, the proportions of PA and SA were very similar for all vegetable and fruits seed oils, with variations between 6-9% for PA, and 2-4% for SA. However, other studies found that PA in tomato and olive seed

oils reached up to 17% and 20% of total FAs, respectively [47, 48] (Table 1).

3. TRADITIONAL AND EMERGING EXTRACTION TECHNOLOGIES OF OMEGA-3 FATTY ACIDS

The most common lipid extraction methods traditionally used from food-related matrix are solvent extraction (SE), Soxhlet extraction (SxE), Wet Pressing (WP) and Cold Pressing (CP) [88, 89]. At present, it is pursued the development of environmentally friendly extraction techniques since the sustainability of the processes to recover bioactive compounds is of the utmost importance [90]. Following this trend, some modern or greener extraction methods have emerged, including microwave-assisted extraction (MAE), ultrasound-assisted extraction (UAE), pressurized liquid extraction (PLE) and supercritical fluid extraction (SFE) [91]. In general, these techniques have some important advantages, such as lower organic solvent consumption, shorter extraction time and greater selectivity, as well as great versatility and efficiency [92]. The main conventional and non-conventional methods for the recovery of oils rich in ω 3 FA are shown in Table 2 and represented in Figure 2.

3.1. Conventional extraction methods

3.1.1. Solvent extraction

Solvent extraction (SE) can be considered the most common extraction method nowadays used for recovering lipids from different food matrices such as fruits, vegetable oils, seeds, nuts, animal fats, and fish oils [93]. Both Folch [94] and Bligh & Dyer methods [95] are the most widely used SE resulting in yields higher than 95% [96]. The Folch method is performed by a mixture of chloroform and methanol (2:1, v/v) and is based on the solubility of lipids in organic solvents and their insolubility in water, allowing them to be separated into insoluble (lipids) and soluble (proteins, carbohydrates and minerals) components [97]. On the other hand, the Bligh and Dyer methodology applies a mixture of chloroform: methanol: water (2:2:1.8, v/v) in a two-step extraction protocol [95, 98]. In terms of applicability, Folch method can be used to extract lipids from most foods matrix, whereas the Bligh & Dyer procedure, initially developed using cod muscle, can be now applied to any tissue containing 80% water (e.g. tissues of vascular plants) [93]. Recently, it has been reported that a single FA extraction using a chromatographic column with chloroform, methanol and water, is a solid, easy and cost efficient alternative to Folch method for salmon and chicken samples analyses avoiding centrifugation and pipetting steps [99]. However, the large amounts of residual toxic solvents (chloroform and methanol) are of supreme concern for the health and safety of chemical sector workers and for the environment [100, 101]. In addition these techniques entail other limitations like the time and energy consumption [75, 96]. Thus, SE is nowadays used for analytical purposes but not for industrial production, due to restrictions in the food industry. To overcome the toxicity of chloroform, alternative solvent systems have been developed with hexane, ethyl acetate and isopropanol, however these are usually less efficient [93].

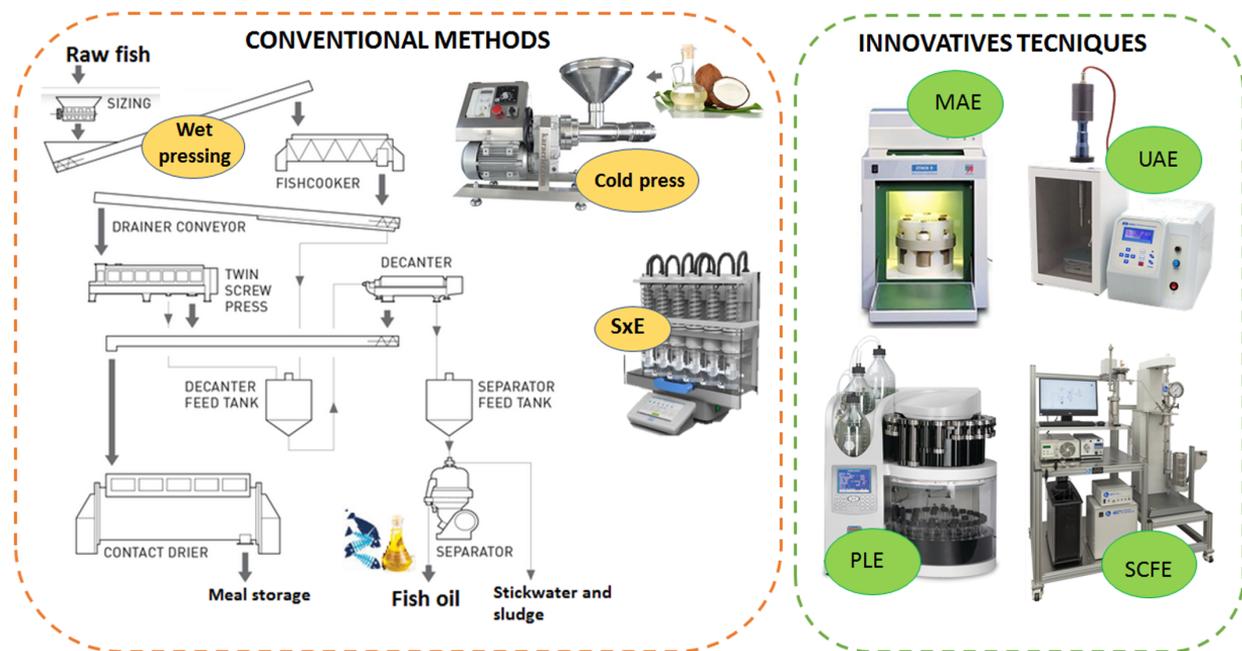


Figure 2 | Traditional extraction of oil versus innovative techniques.

3.1.2. Soxhlet extraction

Soxhlet extraction (SxE) is a conventional technique used for the recovery of lipids from food employing organic solvents such as hexane and petroleum ether. In fact, Soxhlet set-up is the commercial extraction method of Palm-pressed Mesocarp Oil employing hexane. It has been used in palm oil mills in a solvent reflux system that continuously extracts the oil for 4–6 h [102]. Sahena and co-workers employed petroleum ether in a 6 h process to obtain ALA, EPA, DPA and DHA, from flesh, skins, viscera and head of mackerel *Rastrelliger kanagurta* [71]. Also, SxE using petroleum ether (5h process) was applied to almond, apricot, cashew, hazelnut, peanut, pistachio, pecan and walnut to obtain ALA [70]. SxE procedure is very simple, When the powdered solid sample is placed in the cartridge of porous material in the Soxhlet extractor chamber, flask is heated. Then, the solvent evaporates and moves up to the condenser extracting the fats and carries them into the flask [91, 103]. Despite its simplicity, it has some disadvantages: long extraction times, large quantities of extraction residues, flammable organic solvents and the possibility of thermal decomposition of thermolabile compounds due to the high temperatures generated during the process [93, 103]. Thus, several modifications to the process have been developed to improve its efficiency and automation [104]. With the application of auxiliary energies such as UAE or MAE, the efficiency of this technique has been increased [4].

3.1.3. Wet pressing

Wet pressing (WP) is the most widely used method for fish oil production at industrial scale. It is basically carried out in four steps: fish cooking (85–95°C), pressing the cooked matrix, decantation and centrifugation to recover the oil [66]. Subsequently, to produce edible oils, fish oil undergoes a refining process to remove

impurities, such as non-triglyceric compounds, dyes, odorous and toxic compounds. Several European companies, mainly in Iceland, Norway, Denmark and Spain, produce fish oil using WP [101]. This traditional process of obtaining fish oil yields good results by using fish products or their by-products with a high oil content, such as herring, tuna, sardine, and salmon. However, it is not as feasible when the oil content is low [101]. And this technique is often used for fish oil extraction processes, even though it is not always the optimal choice [66]. In addition, WP has other several drawbacks. It involves the use of chemicals that pollute the environment and some neutral oil is lost [101, 105]. WP is an energy-intensive process [105] and the high temperature and pressure conditions used for protein coagulation and further oil release may partially modify the PUFAs content due to the hydrolysis and oxidation reactions [97].

3.1.4. Cold pressing

Cold pressing (CP) extraction is a type of mechanical press method which is carried out at low temperature (below 50 °C) and pressure [106]. It is used to extract oil from a range of matrices like soybean, rapeseed, corn, grapeseed, hemp, flaxseed, rice bran, olive, nut, wheat and pumpkin [88, 107], but is especially used in oil production from oilseeds. CP is often used in rural areas due to the low initial investment cost and the non-requirement of highly trained personnel to operate the machines. CP can be an economical method as it not only excludes the use of heat but also organic solvent. However, one of the disadvantages of this technique is low yields obtained. For example, yields of Virgin Coconut Oil obtained by CP are about 46–49% [102]. Another disadvantage of this technique is the difficulty to obtain a highly quality product [88]. A study showed the amount and the characteristics of the oil extracted from salmon by-products which resulted in high content of ω 3 FA, EPA and DHA (22:6 ω 3) but with yields of 8.60–

21.00% [108]. Although extraction methods especially for the more conventional oilseeds are known, there has been a continuous quest by researchers to improve extraction yields.

3.2. Innovative extraction methods

3.2.1. Microwave-assisted extraction

Microwave assisted extraction (MAE) is one of the most novel and attractive alternative oil extraction methods. It combines solvent extraction with microwave heating power, so that heated solvent gets in contact with the solid matrix to extract the compounds of interest from sample solution [92]. In recent years, there has been an increase in reports of rapid and high-quality MAE extraction of oilseeds [59, 109], fish by-products [55, 56], yeasts [110] and microalgae [63, 111]. For example, it was feasible to obtain oil rich in EPA and DHA from liver of catfish and oil rich in ALA from seeds of purslane and Olive aglandau [57, 58]. MAE consumes a minimum amount of solvent, energy and time due to the rapid and homogeneous heating of the solvent, the generation of high pressure leading to cell rupture and the release of active components from broken cells [112, 113]. Many factors influence the extraction efficiency such as particle size, solvent, time, and microwave frequency [92]. MAE is highly selective, depending largely on the nature of the solvent and the matrix (Castejón et al., 2018) so that it is suitable for oil extraction when employing the proper combinations of solvent. Generally, water is not used while hexane is combined with other different solvents, leading to the extraction of polar and non-polar FAs [100]. However, it has been reported a low MAE efficiency when target compounds or solvents are non-polar, or when they are volatile [78].

3.2.2. Ultrasound-assisted extraction

Ultrasound-assisted extraction (UAE) has been widely applied by food, nutritional and pharmaceutical industries to obtain bioactive FA. UAE requires small amount of solvent and energy and the temperature and extraction time are significantly reduced compared other conventional methods [114]. UAE is based on high-energy ultrasound waves passing through the liquids and creating high/low-pressure cycles, resulting in the phenomenon of acoustic cavitation that leads to cell rupture, intensifying solvent penetration and improving mass transfer between the intercellular materials and the solvent [91, 115, 116]. UAE has been applied for oil extraction from seeds (Castejón et al., 2018; ; Villanueva-Bermejo et al., 2019) [59] and microalgae [4]. In papaya and flax seeds, it was used with hexane to obtain oil suitable for dietary oil products rich in OA and ALA, respectively [60, 117]. However, it is barely employed for the extraction of fish oil [92]. This technique can also be used as pre-treatment before the main extraction process. A recent study shows UAE as a pre-treatment to remove mucilage from chia seeds, which are usually difficult to extract using polar solvents [118]. UAE was combined with other techniques to increase FA extraction efficiency. For example, an aqueous enzymatic process assisted by UAE was applied to the extraction of linseed oil (*Linum usitatissimum* L.), for obtaining an oil richer in PUFAs than that obtained using the conventional solvent extraction method [61]. Also, the combination of UAE

with MAE for the extraction of DHA-rich oils from microalgae has been studied, concluding that both technologies used alone or in combination could reduce costs and improve the rate of extraction and yield compared to conventional extraction [63, 119].

3.2.3. Pressurized liquid extraction

Pressurized liquid extraction (PLE) has already been explored as the extraction technique for a variety of bioactive compounds from food-related by-products, from agricultural and food industry sources, mostly focused on vegetal products [90]. PLE uses solvents at high temperatures and pressures, always below their respective critical points, so that the liquid state of the solvent is maintained throughout the extraction process [90, 120, 121]. Due to these pressure and temperature conditions, the surface tension of the solvent are reduced while the solubility of the analytes increases, allowing a easier solvent penetration and resulting a in faster extraction processes while requiring small amounts of solvents [121, 122]. Besides, PLE is a versatile technique since high range of solvents that can be used, including ethanol, ethyl acetate, ethyl lactate, D-limonene or hexane. When involves the use of water as solvent, technique is called subcritical water extraction (SWE) (Castejón et al., 2018). For the extraction of facts, low- or medium-polarity solvents such as hexane, D-limonene, ethyl acetate, methyl acetate or ethanol are generally used at temperature ranges from 90 to 220°C [122–124]. PLE applied for FAs extraction from *Laminaria ochroleuca* using hexane, ethyl acetate, ethanol, and ethanol/water (1:1) showed that both ethyl acetate and ethanol enriched USFA in the lipid fraction of *L. ochroleuca*, providing extracts up to 55% of their total FA content compared to other solvents [76]. Different PLE extraction conditions of ω 3-rich oil from *Echium plantagineum* L. seeds were recently evaluated, allowing to obtain similar oil yield (31.2%) to SxE (hexane, 8 h) at optimum PLE conditions (150°C ethanol, 10 min) and higher yields compared to MAE (21.2%) and UAE (29.1%) (Castejón et al., 2018). Similarly, a study examined the PLE of wheat germ oil showing a decreased in the solvent consumption and extraction time compared to the SxE while the ω 3 and ω 6 FA composition of the extracts was not affected by either temperature or extraction method [72].

3.2.4. Supercritical fluid extraction

Supercritical fluid extraction (SFE) has attracted interest for developing lipid extraction protocols, both for analytical and industrial applications [4]. Supercritical status is achieved when the temperature and pressure of a substance rise above its critical value, and fluid behave as a hybrid between a liquid and a gas [90]. Supercritical fluids show better mass transfer than liquids, due to their low viscosity and higher diffusivity properties, reducing the extraction time and providing higher extraction yields [97, 116]. Another major advantage of SFE is the reduced use of organic solvents (zero in many cases) allowing the use of non-toxic solvents, such as carbon dioxide (CO₂). In fact, it is the most commonly used extraction solvent (SC-CO₂) [122, 125]. CO₂ has easily achievable critical conditions (30.9°C and 73.8 bar), is easily separable from the solute, does not cause environmental problems; is non-flammable, non-toxic and inexpensive [126]. Its main limitations are the separation of polar compounds, and its high requirements in terms of expensive equipment and energy

consumption to achieve supercritical pressures (Taher et al., 2020;) [127]. SC-CO₂ has been established as an alternative to solvent extraction for lipids, for example, for the extraction of PUFAs from fish and vegetable oils [84]. Since CO₂ is non-polar, less or non-polar isomers forms of PUFAs can be extracted more efficiently, compared to polar forms [100]. The reported ω 3 PUFAs contents in the extracted oil differ depending on the FA profile of the matrix, whereas some studies show that ω 3 PUFAs content is not affected by the extraction method [105].

4. PURIFICATION METHODOLOGIES FOR OMEGA 3 FATTY ACIDS

In recent years, purification methods have been developed to isolate or concentrate ω 3 PUFAs from different oils. The first step is to convert natural triglycerides into ethyl esters (EE) or free fatty acids (FFA) with ethanol [101]. Only when EE or FFA are separated from the main glycerol chain can their concentrations be enriched [128, 129]. Current methods for ω 3-FA purification include molecular distillation (MD), enzymatic enrichment, low temperature crystallization, urea precipitation, supercritical fluid chromatography (SFC) and high resolution liquid chromatography (HPLC) [101]. Applying these methods individually, it is feasible to achieve concentrations up to 30% of EPA and DHA from marine oils [130]. However, when these protocols are used together (e.g., adduction of urea followed by multiple rounds of MD), the concentration of PUFAs increased up to 85% purity [131]. Furthermore, SFE can be used as a concentration method: the higher the molecular weight of the FA, the less solubility in SC-CO₂. SC-CO₂ can also be used for the selective separation between all C18, C20 and C22 FAs [132]. Unfortunately, it has been established that the selectivity of SFE of PUFA is only based on the number of carbons of the chain, but not on the number of double bonds. SFE should therefore be combined with other techniques, such as urea complexation [133]. Currently, the purification technology used at industrial scale with the ability to provide consistently high purity EPA or DHA (> 95%) is based on liquid chromatography (LC) and SFC [131].

4.1. Liquid Chromatography (LC)

Liquid Chromatography (LC) is, together with SFC, the most selective separation technique, discriminating both by the length of the chain of FAs as well as by their degree of unsaturation, [130]. Several types of LC can be applied, depending on the stationary phase used: high performance liquid chromatography (HPLC), liquid-solid chromatography (LSC), liquid-liquid chromatography (LLC) and reverse-phase chromatography (RP) [134]. HPLC reach purities above 90%. RP-HPLC plays a key role in the analysis of long-chain PUFAs, allowing the separation of those FAs that cannot be separated by normal phase HPLC [135, 136]. The main drawback of HPLC is the poor resolution for complex mixtures and the low sensitivity, although this can be avoided by using mass spectrometry (MS) [137]. The application of HPLC coupled to mass spectrometry (HPLC-MS) is relatively recent, but suitable for the precise determination of PUFAs [138]. Numerous ionization and detection modes can be applied for FAs analysis such as electrospray ionization (ESI), atmospheric pressure chemical ionization (APCI),

or time of flight (TOF) [138–140]. Also, the use of tandem mass spectrometry (HPLC-MS/MS) provides a more specific detection of the FAs and their derivatives, being able to determine the position of the double bonds or the ramifications in the FA chain (; Volpato et al., 2017) [138]. Another common method is silver ion chromatography (Ag-HPLC), which uses embedded silver ions in the stationary phase [141]. In Ag-HPLC, triacylglycerides are separated according to the number, geometric configuration and position of the double bonds, increasing the retention as the number of double bonds increases [131, 142]. At last, another disadvantage of LC is the generation of large volumes of toxic solvents that need to be removed from the isolated FA, often causing oxidative stress in PUFAs [128].

4.1.1. Supercritical Fluid Chromatography (SFC)

Supercritical Fluid Chromatography (SFC) uses supercritical fluids, usually CO₂ as mobile phase instead of the toxic organic solvents used in LC [101, 143]. SFC is considered a hybrid of gas chromatography (GC) and HPLC, presenting many advantages over these two methods, such as high separation efficiency, low consumption of organic solvents and short separation time [144]. SCF is used at an industrial scale, allowing up to 99% of pure individual FAs. This high selectivity is achieved by the separation according to the chain length and the number of double bonds of the FAs. Due to the low viscosity of supercritical CO₂, the use of long chromatographic columns filled with highly selective filler material can be employed. In addition, working temperatures between 40-50°C prevent thermal stress in EPA and DHA. SFC is therefore considered one of the most appropriate technologies for the concentration of ω 3-FAs [128]. SFE allows the use of universal detectors such as flame ionization detectors (FID), evaporative light dispersion detectors (ELSD) or MS, providing very good sensitivity levels when combining SFE, SFC and MS [137, 139]. The SFE/SFC coupling offers the advantages of each method: SFE can selectively extract the fraction of FAs whereas SFC can eliminate any organic solvent that remains from the procedure [145].

5. FATTY ACIDS ENCAPSULATION AND INCORPORATION IN FOODS

Food industry has developed different encapsulation techniques using diverse shell materials which have allowed obtaining capsules with variable physical properties. This variability in the process has permitted to adequate the type of capsules for protecting a huge variability of core ingredients. Encapsulation prevents the biological and physicochemical degradation of the biocompounds and improves their chemical stability and hence protects their bioactivities. Besides, encapsulation may also allow the controlled release of very specific concentrations of the biocompounds. Scientific literature provides several examples of different FA which have been encapsulated to improve the nutritional value of food matrixes and, in some cases, to extend their shelf-life.

5.1. Emulsions

Emulsions are created by the agitation of at least two immiscible liquids, such as water and oil. This mechanical process generates heterogeneous mixtures in which fine droplets of the dispersed phase are uniformly spread throughout the continuous phase. The stability of emulsions is quite low since phases can get newly separated. To improve the stability and emulsion efficiency different (co-) surfactants or emulsifying agents can be utilized. Food-grade emulsifying agents employed in food industry for FA mainly include protein- or polysaccharide-based ingredients such as whey, gelatin, casein, lecithin, Arabic gum, chitosan, maltodextrin, or pectin [146, 147]. Obtained droplets by emulsification can possess very variable diameters although, those created with industrial purposes usually have a range between the nano (nm) and micro (μm) scale [148]. They can be achieved by following simple steps based on stirring/sonication or by using specific techniques, such as microfluidization, that require the application of high pressure through microchannels, high-energy inputs and specific instruments but it produces ultrafine emulsions at very low surfactant-to-oil ratios [147].

Emulsions with thermal and thermodynamic stability have been proved to increase the bioavailability of the core ingredients. That is because emulsions prevent from direct exposure to chemical, enzymatic and/or physical agents, especially, during food processing. Hence, they improve not just the bioavailability, but the bioaccessibility and bioactivity of core ingredients, besides they provide a tool to control their release (Ricaurte et al., 2016, 2018). Based on these benefits, food industry has tested the performance of many core ingredients emulsified with several surfactants into different matrixes. Among the assayed food matrixes, meat and dairy products are the most usual targets (Table 3). The application of emulsions is mainly meant to reduce fat content, especially saturated lipids, and/or to extend their life-shelf but without altering the organoleptic properties of the product.

Several works have demonstrated the viability and benefits of replacing animal fats with vegetal ones in different meat matrixes. For instance, freeze-dried pineapple by-product and canola oil were used to replace fat content in beef burgers. This treatment was showed to improve the lipidic profile by reducing saturated fats from 31 to 27g/100 g, MUFAs increased from 45 to 53g/100 g and PUFAs from 13 to 15g/100g. This alteration of the fat profile provided a reduction in the ω_6/ω_3 ratio, and therefore in the atherogenic and thrombogenic indexes. Therefore, the emulsion containing a mixture of canola oil and pineapple by-product was considered a useful fat replacer capable of providing a healthier kind of burgers [149]. *Salvia hispanica* (chia) and *Avena sativa* (avena) were also used to crease emulsion gels ant to partially replace animal fat in a class of sausages named after “longaniza”. The composition of cooked sausages showed a higher PUFAs content, especially in sausages incorporated with *S. hispanica*. In general terms, the inclusion of these vegetal-based emulsions significantly minimized the weight loss during grilling and also increased lightness, lipid oxidation and texture of sausages [150]. In beef sausages the total or partial replacement of animal fat was performed with pre-emulsified hazelnut oil and powder with no apparent sensorial alterations. This approach displayed a reduction into the content of SFA (from 47 to 14%) accompanied of an increment of MUFAs (from 42 to 71%)

and PUFAs (from 4 to 11%). This alteration in the lipidic profile of sausages was revealed to be healthier since it provides low indexes of atherogenicity and thrombogenicity [151]. Different emulsion gels containing different ratios of soy protein, carrageenan and inulin were also tested to replace animal fat in frankfurters. Reformulated frankfurters presented a reduction of 53% of SFA while increased the amount of PUFAs. Again, this shift in the FA profile leads to the reduction of the atherogenicity and thrombogenicity indexes which newly indicates the health benefits that involves this fat replacement [152]. The effect of inverse emulsions of water/oil and carrot powder was assayed into beef meat batters. Their use reduced the saturated fat content from 46 to 17% with an increment in MUFAs from 51 to 72% and in PUFAs from 2 to 10%. Color shifts induced by emulsions were counteracted by carrot powder that also provided antioxidant capacity [153].

Dairy products, mainly yogurts, have been also fortified using emulsified ingredients. Nanoemulsions of sweet almond and sesame oil tested in yogurt showed to be able to decrease pH and syneresis degree and to increase acidity, malondialdehyde formation, and antioxidant activity. The addition of the emulsions slightly modified the yogurt viscosity and the sensory acceptability. However, they were demonstrated to reduce the content of saturated fats to half, MUFAs can be nearly doubled and PUFAs can be increased to more than 10-folds. Therefore, these emulsions were considered positive in terms of health benefits despite the sensorial alterations they induced [154]. *Phoenix dactylifera* pollen grains were used to fortified yogurt by direct addition of the grains, or by the addition of a free ethanolic extract 80% or its encapsulated form. This vegetal matrix was selected for its high nutritional content (proteins, carbohydrates, and minerals) which also revealed it as a source of PUFAs and MUFAs and antioxidants (phenolic compounds, mainly catechins). These properties permitted to reduce the amount of saturated fats while increasing PUFAs and MUFAs, which prompted a slight increment in the ω_6/ω_3 -ratio. Among the three fortification strategies, the nanoencapsulated showed a more similar yoghurt microstructure to the control, it reduced syneresis and viscosity, increased the water holding capacity and did not modify the yogurt color [155]. Similar results were obtained in an experiment into which a nanoemulsion of fish oil and γ -oryzanol was added to yogurt. The nanoemulsion reduced the acidity and syneresis of yogurt and the fortification meant a huge increment of PUFAs due to the significant amount of EPA and DHA in fish oil. These ω_3 PUFAs usually get easily oxidized however the use of nanoemulsion reduced the oxidative environment and showed low peroxide values. Even though, the sensorial panel and the viscosity of the final product were not as good as the plain yogurt the introduction of optimized nanoemulsions seems a promising strategy to fortify dairy products [156].

Apart from their use for fortifying food matrixes, nanoemulsions have been also included in films becoming active packaging even with biodegradable properties. The fibrous film into which nanoemulsions containing high oleic palm oil were embedded was described to be capable of extending shelf- life products and decreasing storage costs while using an innovative product with application for any lipidic product [157].

5.2. Encapsulation: spray-drying

In food industry very different strategies, with diverse complexity degrees, have been developed to encapsulate a huge variability of biocompounds [9]. FA are encapsulated with the final aim of preserving them against oxidation processes triggered by external factors such as humidity, light, or temperature [158]. Some of the most used encapsulation methods include spray or freeze drying, spray chilling and cooling, coacervation, fluidized bed coating, liposome entrapment, rotational suspension separation, extrusion and inclusion complexation, etc. [159]. Among them, the most widely applied for encapsulating FA is spray drying together with freeze drying (Table 3). However, the high-quality and high efficiency rates, its flexibility and easy handle make spray drying an economical and affordable encapsulation technique despite the high consumption of energy it requires [158, 159].

Very different FA have been spray-dried encapsulated and utilized for fortifying food matrixes, mainly meat, bakery and dairy products (Table 3). For instance, the oil extracted from *Salvia hispanica* (*S. hispanica*) is well known for its high content of ALA, an ω 3 PUFA with beneficial health properties but with a high auto-oxidation ratio too. To prevent this oxidation, the obtained oil was encapsulated by spray drying using chitosan as shell material and used to fortify butter at different levels. This type of microcapsules resulting in an increment of 17% of the PUFAs content, providing high antioxidant activity that nearly reached 70% after 90 days of storage and without affecting the sensorial properties of the butter [174]. Parallely, the oil extracted from *Lepidium sativum* seeds has also been demonstrated to possess high levels of ALA and it is also used for fortifying food products. One study shows the oil microencapsulation by spray drying using whey as well ingredient to fortify biscuits, resulting in a slightly reduction of ALA oxidation and an improvement of the lipidic profile of the biscuits with an acceptable organoleptic properties from a sensorial point of view [175].

In addition, different works have taken profit of the encapsulation of fish or shrimp oil to mainly fortify dairy products and meat (Table 3). For instance, three different cheese classes named after queso fresco, cheddar, and mozzarella were fortified with ω 3 PUFAs obtained from flaxseed oil or fish oil. Fish oil was microencapsulated for masking its organoleptic properties but maintain its nutritional properties. The fortification of the cheddar cheese modified some physicochemical properties and textures but was the cheese class that suffered fewer alterations. Cheddar was the cheese that showed higher ω 3 PUFAs retention, up to 9 mg/g, and around 5 mg/g for ω 6. This high retention of PUFAs means that the daily consumption of a portion of this cheese (50–100 g) can supply the recommended amount of ω 3 in order to prevent the development of cardiovascular diseases. Therefore, the optimization of fish oil fortification of cheese represents a very promising strategy to provide functional properties with health benefits [176]. In other dairy products such as yogurts, micro- and nanocapsules containing fish oil seems to have neutralized fishy odors and flavors. In a study yogurt was fortified utilizing nano-liposomes to nano-encapsulate fish oil. As observed in works cited above, the inclusion of the nanocapsules reduced the acidity and syneresis but also the peroxide value along for weeks. Besides, this fortification resulted in an increment of the amount of DHA and EPA while mostly preserving the

sensory properties of the yogurt fortified [177]. Similarly, in a previously published work, a strawberry yogurt was fortified using microencapsulated salmon oil. In this case, the addition of the microcapsules did not affect to the acidity, syneresis, color or water-holding capacity. The oxidation of the yogurt, mainly triggered by its time storage, was not prevented by the fortification. However, the values of thiobarbituric acid that both samples, control and treated, reached were kept low which avoided sensorial alterations. The addition of microcapsules modified the lipidic profile of the yogurt, even after one month of storage. The amount of saturated fatty acids was reduced from 66 to 58% while MUFAs were incremented from 28 to 32% and PUFAs from 6 to 10%. The improved fatty acid profile of the fortified yogurt demonstrates the benefits of using fish oil to provide more healthy options to consumers [178]. Also skim milk has been fortified with nanoliposomes loaded with shrimp oil showing no sensorial alterations related with the use of marine products. Besides the fatty acid profile of this fortified milk showed similar content of saturated and PUFAs (about 39g/100g of lipids) and a high presence of MUFAs (20g/100g of lipids) [179].

Therefore, as demonstrated with these examples, emulsions or encapsulation represents a very useful tool for improving the nutritional value of products and represent a huge benefit to exploit the use of fish or agriculture by-products derived from marine or horticulture activities. The strong flavor and/or odor that they usually possess can be masked by their encapsulation which permits to exploit them as a sustainable source of very interesting FA.

6. FUTURE TRENDS AND MAIN CHALLENGES

FAs have been used in many different fields due to their potential applications, from environmental purposes to food science functions. In the food industry, FAs are mainly used as supplements since supplementing food with ω 3 or its use for pharmaceutical applications are feasible options for complementing the optimum dietary intake [2, 180]. In a similar way, other studies in animal feed opt for supplementing animals' diet to get a better FA profile [181]. Some of the most recent studies include the supplementation of *Oreochromis niloticus* fillets with fish oil which causes a significant reduction of ω 6/ ω 3 ratio (Duarte et al., 2021). More recently, FAs have shown their potential as coagents to treat tuberculosis in mice administrated with LA, ALA, EPA and DHA for 3 days. At the end of the treatment, the mice showed lower ω 6/ ω 3 ratio and lower levels of pro-inflammatory interleukins (IL-1 α , IL-1 β and IL-6), thus being potentially applicable to the pharmaceutical industry [182].

By-products from the fish, crustacean, cereal and fruit and vegetable industries have been revealed as a source of high-value FAs [23, 183]. For the efficient recover of these compounds, it is essential to know the total content of FAs in these by-products as well as the perfect extraction and purification techniques aimed at optimizing their recovery. From available extraction methods, MAE and UAE are still in the process of being applied to by-products processing [100]. On the other hand, the most recent approaches are focused on Enzyme Assisted Extraction (EAE) or SC-CO₂ combined with other clean fractionation techniques. EAE is an enzymatic hydrolysis method that use exogenous enzymes to makes digestion process better controllable and reproducible [92].

Table 3 Applications of encapsulated FAs with marine and terrestrial origin. FAs extracted from different sources and encapsulated with diverse shell materials and techniques have been applied to different kind of matrixes to improve their quality properties.

Fatty acid source	Shell material	Encapsulation strategy	Matrix	Properties	Ref
Fish oil	Lecithin-chitosan and maltodextrin	ME by spray drying	Chicken nuggets	Improvement of oxidative stability and preserving sensory quality	[160]
Fish oil	Konjac glucomannan	ME by spray drying	Spanish “salchichón”	Fat content reduction (30%), PUFA increment (2%) but also lipid oxidation and altered sensory quality	[161]
Fish oils	Sodium caseinate	ME by freeze drying	Ice cream	Alteration of lipidic profile: SFA from 65 to 46%, MUFA 28 to 38% and PUFA 1 to 3%	[162]
Fish oil	Not indicated	ME	Microcapsule powder	Increment of long chain ω 3 PUFA concentration in blood patients	[163]
Fish oil	Lecithin-chitosan and maltodextrin	ME by spray drying	Pork meat burgers	Enrichment of pork meat with PUFAs, prevention of oxidative reactions and organoleptic acceptance	[164]
Microalgae	Maltodextrin, gum acacia, sodium caseinate, starch	Spray drying	Fruit juice	Enhancement of bioavailability, shelf life and oxidative stability	[165]
Chia oil	Carnauba wax and sodium caseinate	ME by freeze-drying	Cookies	Increment of ALA to 48%, AI and TI reduction. Sensory acceptance.	[166]
Flaxseed oil	Under patent	ME	Ice cream	Increment of ALA. Fresh ice cream (100 g) meet ~45% RDA ALA, at day 120 of storage it meets ~35%	[167]
Flaxseed oil	Gelatin, gum Arabic, lactose, transglutaminase	ME	Milk	Improvement of oxidative stability but alteration of sensory properties	[168]
Flaxseed oil	<i>Saccharomyces cerevisiae</i> cells and β -glucan	ME by freeze-drying	Bread	Reduction of the peroxide index, increment of ALA content, preservation of sensory properties	[169]
Chia, linseed and chufa oils	Sodium caseinate and lactose	ME by spray drying	Deer pâté	Reduction of cholesterol and SFA, increment of MUFAs and PUFAs, modification of color and textures, but higher oxidative instability	[170]
Virgin coconut oil	Soy protein and lecithin	Emulsion	Biodegradable film	Active packaging with antioxidant capacity in olive oil storage	[171]
Clove oil	Chicken feather protein/pork gelatin	Embedded in protein/gelatin matrix	Gelatin film	Antioxidant and antimicrobial when used for storing smoked salmon	[172]
Cinnamon, rosemary and basil EOs	Whey protein	Embedded in whey protein matrix	Biodegradable film	Antioxidant and antimicrobial activities in fatty food simulant	[173]

Abbreviations: AI: atherogenic index, ALA: α -linolenic acid, EOs: essential oils, ME: microencapsulation, MUFAs: monounsaturated fatty acids, PUFAs: polyunsaturated fatty acids, RDA: recommended dietary allowance, SFAs: saturated fatty acids, TI: thrombogenic index.

Thus, enzymatic hydrolysis is being an ideal way to recover oil from fish and fishery processing wastes with suitable enzyme and water. In most cases, alkaline/neutral proteases are used for the hydrolysis because they produce better results than the acidic proteases. The benefit of this method is can obtain large amount of oil compared to others methods due to the presence of enzymes that can catalyze the hydrolysis reaction process [184]. In addition, some of the last studies of SC-CO₂ in a pilot-scale has revealed to be a promising process for the extraction of high amounts of oil from Colombian mango seed kernel, reaching oil yields of 83 g/kg at 37 MPa and 63°C and an EFARich lipid fractions in LA (37 g/kg) and ALA (4 g/kg) acids [185].

Besides, from another perspective, the composition of the by-products must be considered. The content of PUFA in plant seeds are being investigated as source of PUFA, however the

concentration is lower than fish oil due to the absence of biosynthetic route in plants to produce DHA and EPA. Considerable efforts have been made to improve the composition of vegetable oil, and attempts have been made in producing DHA and EPA in plants by using algal, yeast, and bacterial genes involved in the PUFA synthesis [12]. Therefore, some studies are focused on the role of microorganisms and lipolytic enzymes over these products, as is the case of whole-crop oat silages and the alterations of the FAs profile motivated by these microbes [186]. On the other hand, a recent study used acidogenic fermentation to produce volatile FA from household food waste [187]. This way it could be used as a potential tool to manage this type of residues that are continuously growing. Taken all together, the utilization of agriculture and aquaculture by-products as a source of FAs still needs to face some challenges, mainly directed towards the optimization of the extraction and purification techniques and the improvement of the encapsulation

and incorporation methodologies.

7. CONCLUSIONS

The search for economic and sustainable sources of PUFAs following the standards of circular economy is encouraged by their proven beneficial effects on health. The EFAs commercial products, represented by DHA and EPA, mainly derived from fish oil. Marine fishes are high in $\omega 3$ FAs, however high consumption of those fishes will cause a shortage of fish stocks existing naturally in the oceans. The search for alternative sources to get the recommended daily intake of $\omega 3$ FAs is the trend of today. There is a demand of more sustainable and cheaper $\omega 3$ sources like seeds. In addition, by-products from the fish, crustacean, cereal and fruit and vegetable have been revealed as a source of high-value FA $\omega 3$ (DHA, EPA, ALA) and $\omega 6$ (LA), being a potent biomass to successfully develop additives rich in $\omega 3$ and useful to maintain the good ratio $\omega 6$ to $\omega 3$. Their applications will be probably connected to the optimum dietary intakes of FAs and future personalized nutrition by new formulations and functional foods. Thus, these strategies not only ensure more sustainable process, but also put in value new resources to extract and obtain different FA which could be further employed in the development of new industrial products without producing more wastes and economic losses

Oil extraction methods from food and food wastes include the traditional methods (ES, SxE, WP and CP) and improved nonconventional techniques (MAE, UAE, PLE, SFE and EAE) which have the potential to improve oil extraction yields while reduce extraction times and minimize deterioration of the oil quality. However, the majority studies carried out on the nonconventional methods of oil extraction have been focused on laboratory analyses. There is a need to extend the research and to scale up to industrial systems. As by-products have different nature, the FA extraction process needs to ensure the suitability of the technology from an economical and technical point of view. After extraction, LC fractionation allows to separate the oil components of interest according to their polarity and molecular weight, which are usually applied for the purification of $\omega 3$. The emulsion and encapsulation of FAs has been revealed as a promising tool to protect them from external agents involved in their fast oxidation and thus, it extends their chemical stability. Once stabilized, the nutritional properties of FA can be used to fortify different food matrixes to improve their lipidic profile. Besides, the use of these protective shells can be used to mask the odor or flavor that some FA possess and wider their applications while preventing negative sensorial impacts.

8. ABBREVIATIONS

Generic

FAO Food and Agriculture Organization of the United Nations

EE Ethyl Esters

ns Not specified

Fatty acids

FA Fatty Acid

FFA Free Fatty Acids

USFA Unsaturated Fatty Acid

MUFAs Monounsaturated Fatty Acids

PUFAs Polyunsaturated Fatty Acids

$\omega 3$ Omega-3

$\omega 6$ Omega-6

GLA γ -linolenic acid

ALA α -Linolenic acid

DHA Docosahexaenoic acid

DPA Docosapentaenoic acid

EFAs Essential Fatty Acids

ETA Eicosatetraenoic acid

EPA Eicosapentaenoic acid

HTA Hexadecatrienoic acid

SA Stearic acid

SDA Stearidonic acid

Extraction and identification techniques

PLE Pressurized Liquid Extraction

MAE Microwave-Assisted Extraction

UAE Ultrasound-Assisted Extraction

EAE Enzyme Assisted Extraction

SWE Subcritical Water Extraction

SFE Super-Critical Fluid Extraction

SC-CO₂ Supercritical CO₂ Extraction

SE Solvent extraction

SxE Soxhlet Extraction

SFC Supercritical Fluid Chromatography

HHPE High Hydrostatic Pressure Extraction

HPLC High Resolution Liquid Chromatography

LC Liquid Chromatography

MS Mass Spectrometry

HPLC-MS High Resolution Liquid Chromatography-Mass Spectrometry

ESI Electrospray Ionization

APCI Atmospheric Pressure Chemical Ionization

TOF Time Of Flight

HPLC-MS/MS Tandem Mass Spectrometry

Ag-HPLC Silver Ion Chromatography

GC Gas Chromatography

FID Flame Ionization Detectors

ELSD Evaporative Light Scattering Detectors

MD Molecular Distillation

CP Cold Pressed

WP Wet Pressing

CONFLICTS OF INTEREST

All authors declare there is no conflict of interest.

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